

## LESSON-6

### SOLVED EXAMPLES ON CONDUCTION

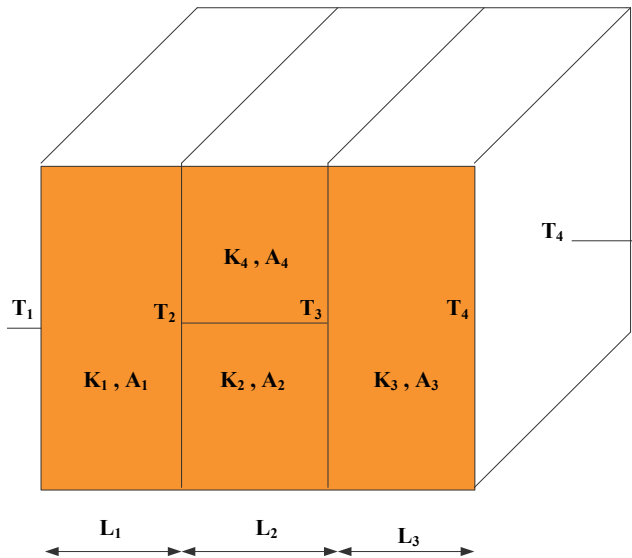
**Ex 6.1** Find the heat flow rate per unit area through a composite wall made of four different materials as shown in Figure 1. Thermal conductivities are as:

$K_1 = 50 \text{ W/m-deg}$ ;  $k_2 = 80 \text{ W/m-deg}$ ;  $k_3 = 150 \text{ W/m-deg}$ ;  $k_4 = 55 \text{ W/m-deg}$

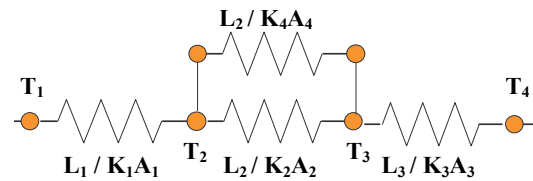
$L_1 = 25 \text{ cm}$ ,  $L_2 = 85 \text{ cm}$ ,  $L_3 = 40 \text{ cm}$ ,  $L_4 = 85 \text{ cm}$ ,

Temperatures on left face and right face are  $525^\circ\text{C}$  and  $50^\circ\text{C}$  respectively.

**Solution:** The arrangement of the composite system and its equivalent thermal circuit for heat flow has been shown in Figures 2 and 3.



**Figure 1**



**Figure 2**

**Given:**  $T_1 = 525^\circ\text{C}$ ,  $T_4 = 50^\circ\text{C}$ ,

Thickness of Ist material,  $L_1 = 25 \text{ cm} = 0.25 \text{ m}$ , Thickness of IInd material,  $L_2 = 85 \text{ cm} = 0.85 \text{ m}$

Thickness of IIIrd material,  $L_3 = 40 \text{ cm} = 0.40 \text{ m}$ , Thickness of IVth material,  $L_4 = 85 \text{ cm} = 0.85 \text{ m}$

Thermal conductivity of Ist material,  $k_1 = 50 \text{ W/m-deg}$ ,

Thermal conductivity of IInd material,  $k_2 = 80 \text{ W/m-deg}$

Thermal conductivity of IIIrd material,  $k_3 = 150 \text{ W/m-deg}$

Thermal conductivity of IVth material,  $k_4 = 55 \text{ W/m-deg}$

$A_1 = A_2 = A_3 = A_4 = 1 \text{ m}^2$

To determine: i) Rate of heat loss per unit area, Q

$$= \frac{\Delta T}{\sum R_t}$$

$$\Delta T = T_1 - T_4 = 525 - (50) = 475^\circ\text{C}$$

$\sum R_t$  is due to thermal resistances,  $R_{t1}$ ,  $R_{t2}$ ,  $R_{t3}$  and  $R_{t4}$

$$R_{t1} = \frac{L_1}{k_1 A_1} = \frac{0.25}{50 \times 1} = 0.005 \text{ deg/W}$$

$$R_{t2} = \frac{L_2}{k_2 A_2} = \frac{0.85}{80 \times 1} = 0.011 \text{ deg/W}$$

$$R_{t3} = \frac{L_3}{k_3 A_3} = \frac{0.4}{150 \times 1} = 0.0026 \text{ deg/W}$$

$$R_{t4} = \frac{L}{k_4 A_4} = \frac{0.85}{55 \times 1} = 0.015 \text{ deg/W}$$

The resistances  $R_2$  and  $R_4$  are in parallel and their equivalent resistance  $R_{eq}$  is

$$R_{eq} = \frac{R_{t2} \times R_{t4}}{R_{t2} + R_{t4}} = \frac{0.011 \times 0.015}{0.011 + 0.015} = 0.0063 \text{ deg/W}$$

$$\text{Total resistance } R_t = \sum R_t = 0.005 + 0.0063 + 0.0026 = 0.0139 \text{ deg/W}$$

$$\therefore \text{Heat loss } Q = \frac{\Delta T}{\sum R_t} = \frac{525 - (50)}{0.0139} = 34.17 \text{ kW}$$

**Ex 6.2** A pipe having inner and outer diameter of 15 cm and 18 cm is carrying hot oil at temperature  $200^\circ\text{C}$ . The pipe is located in a room which is maintained at  $20^\circ\text{C}$  and the thermal conductivity of the pipe material is  $250 \text{ W/(m-K)}$ . Neglecting surface heat transfer coefficients, determine the heat loss through the pipe per unit length and the temperature at a point halfway between the inner and outer surface.

**Solution:**

**Given:**  $T_1 = 200^\circ\text{C}$ ,  $T_2 = 20^\circ\text{C}$ , Inner diameter of pipe,  $d_i = 15 \text{ cm} = 0.15 \text{ m}$ ,

**Outer diameter of pipe,  $d_o = 18 \text{ cm} = 0.18 \text{ m}$**

**Thermal conductivity of pipe material,  $k_1 = 250 \text{ W/m-deg}$ ,**

**Heat transferring area,  $A_i = \pi d_i L = 3.142 \times 0.15 L$ ,  $A_o = \pi d_o L = 3.142 \times 0.18 L$**

L is the length of pipe which is not given but can be assumed to be 1m as heat loss per meter length of pipe is to be determined.

To determine: i) Rate of heat loss per unit length, Q

$$= \frac{\Delta T}{\sum R_t}$$

$$R_t = \frac{1}{2\pi kl} \log_e r_2/r_1 = \frac{1}{2\pi \times 250 \times 1} \log_e(0.09/0.075)$$

$$= 1.16 \times 10^{-4} \text{ deg/W}$$

$$\text{Heat loss } Q = \frac{\Delta t}{R_t} = \frac{200-20}{1.4516 \times 10^{-4}} = 1551 \text{ kW}$$

(ii) Temperature at halfway through the pipe, T

Radius at halfway through the pipe wall, r

$$r = \frac{r_1 + r_2}{2} = \frac{9 + 7.5}{2} = 8.25 \text{ cm} = 0.0825 \text{ m}$$

Thermal resistance of cylindrical pipe upto its mid-plane

$$= \frac{1}{2\pi kl} \log_e(r/r_1) = \frac{1}{2\pi \times 250 \times 1} \log_e(0.0825/0.075)$$

$$= 6.06 \times 10^{-5} \text{ deg/W}$$

Since heat flow through each section is same;

$$1551 \times 10^3 = \frac{T_1 - T}{6.06 \times 10^{-5}}$$

∴ Temperature at the mid plane,

$$T = 300 - 1551000 \times 6.06 \times 10^{-5} = 105.9^\circ\text{C}$$

**Ex 6.3** Determine the rate of heat loss per unit length from an insulated pipe ( $k = 225 \text{ W/m-deg}$ ) of 30 mm inner diameter which is having a thickness of 4 mm and is covered with 20 mm thick insulation ( $k = 0.05 \text{ W/m-deg}$ ). The inside and outside convective heat transfer coefficients are  $10 \text{ W/m}^2\text{-deg}$  and  $5 \text{ W/m}^2\text{-deg}$  respectively. Fluid being carried in the pipe is at  $300^\circ\text{C}$  and air surrounding the pipe is at  $30^\circ\text{C}$ .

**Solution:**

**Given:**  $T_1=300^\circ\text{C}$ ,  $T_2=30^\circ\text{C}$ , Inner pipe diameter,  $d_i=30 \text{ mm}$ ,  $r_i=15 \text{ mm} = 0.015 \text{ m}$ ,  
**Thickness of Pipe = 4 mm, Thickness of insulation = 20 mm,**

Outer pipe diameter,  $d_2 = d_1 + 2 \times \text{Pipe thickness} = 30 + 8 \text{ mm} = 38 \text{ mm}$

$r_2 = 19 \text{ mm} = 0.019 \text{ m}$ ,  $r_3 = r_2 + \text{thickness of insulation} = 0.019 + 0.02 = 0.039 \text{ m}$

Heat transferring area:

$$A_i = 2\pi r_i L \quad A_2 = 2\pi r_2 L, \quad A_3 = 2\pi r_3 L$$

Thermal conductivity of pipe material,  $k_1 = 225 \text{ W/m}^\circ\text{C}$ ,

Thermal conductivity of insulation,  $k_2 = 0.05 \text{ W/m}^\circ\text{C}$ ,

Inside convective heat transfer coefficient,  $h_i = 10 \text{ W/(m}^2\text{-deg)}$

Outside convective heat transfer coefficient,  $h_o = 5 \text{ W/(m}^2\text{-deg)}$

$L$  is the length of pipe which is not given but can be assumed to be 1m as heat loss per meter length of pipe is to be determined.

To determine: i) Rate of heat loss per unit length,  $Q$

$$= \frac{\Delta T}{\sum R_t}$$

The thermal resistances offered to flow of heat are as:

a. Inside fluid film,

$$R_{t_1} = \frac{1}{h_i A_i} = \frac{1}{h_i 2\pi r_1 L} = \frac{1}{10 \times 2 \times 3.142 \times 0.015 \times 1} = 1.06 \text{ deg/W}$$

b. Pipe material,

$$R_{t_2} = \frac{\log_e r_2/r_1}{2\pi k_1 L} = \frac{\log_e (0.019/0.015)}{2 \times 3.142 \times 225 \times 1} = 1.67 \times 10^{-4} \text{ deg/W}$$

c. Insulation,

$$R_{t_3} = \frac{\log_e r_3/r_2}{2\pi k_2 L} = \frac{\log_e (0.039/0.019)}{2 \times 3.142 \times 0.05 \times 1} = 2.28 \text{ deg/W}$$

d. Outside air film,

$$R_{t_4} = \frac{1}{h_o A_o} = \frac{1}{h_o 2\pi r_3 L} = \frac{1}{5 \times 2 \times 0.039 \times 1} = 2.56 \text{ deg/W}$$

$$\sum R_t = R_{t_1} + R_{t_2} + R_{t_3} + R_{t_4} = 1.06 + 1.67 \times 10^{-4} + 2.28 + 2.56 = 5.900167 \text{ deg/W}$$

$$\Delta T = T_1 - T_2 = 270^\circ \text{ C}$$

$$Q = \frac{\Delta T}{\sum R_t} = \frac{270}{5.900167} = 45.76 \text{ W/m}$$

## HEAT GENERATION NUMERICAL

**Example 6.4** An electric heater is providing uniform heat flux to a wall of 5 cm thickness having conductivity,  $k=0.5 \text{ W/(m-deg)}$  so that its outer surface is maintained at  $15 \text{ }^\circ\text{C}$ . The outer and inner surfaces of the wall are exposed to air at  $4 \text{ }^\circ\text{C}$  and  $50 \text{ }^\circ\text{C}$  respectively. Inside and outside convective heat transfer coefficients are  $20 \text{ W/(m}^2\text{-deg)}$  and  $80 \text{ W/(m}^2\text{-deg)}$ . Determine the energy supplied to electric heater per unit area of the wall.

**Solution:**

**Given: Temperature of air in contact with inner surface,  $T_1=50^\circ\text{C}$ ,**

**Temperature of air in contact with outer surface,  $T_a=4^\circ\text{C}$ ,**

**Temperature of outer surface of wall,  $T_{os}=15^\circ\text{C}$ ,**

**Thickness of wall = 5 cm = 0.05 m, Conductivity of wall,  $k = 0.5 \text{ W/(m-deg)}$**

**Inside convective heat transfer coefficient,  $h_i = 20 \text{ W/(m}^2\text{-deg)}$**

**Outside convective heat transfer coefficient,  $h_o = 80 \text{ W/(m}^2\text{-deg)}$**

**Let  $q_g$  amount of energy is supplied to electric heater.**

**To determine: i) Energy supplied to electric heater per unit area of wall,  $q_g$**

From heat balance considerations for unit area of wall, it is clear that the heat gained by the outer surface from inner surface and electric heater is being lost to outside air by convection. Therefore,

Heat gained by outer surface from inside hot air + Heat supplied by electric heater,  $q_g$  = Heat lost by outer surface to surrounding air by convection

$$\frac{(T_1 - T_{os})}{\frac{1}{h_i} + \frac{\delta}{k}} + q_g = h_o(T_{os} - T_a)$$

Substituting the given data,

$$\frac{(50 - 15)}{\frac{1}{20} + \frac{0.05}{0.5}} + q_g = 80 \times [15 - (4)]$$

$$\text{Or } \frac{35}{0.05+0.1} + q_g = 880$$

$\therefore$  Electric power to be provided,

$$q_g = 880 - \frac{35}{0.15} = 646.66 \text{ W/m}^2$$

**Ex 6.5**

**Determine temperature at surface and maximum temperature of a 3 m long wire of diameter 5 mm when a current of 500 amperes is passing through it and it is immersed in a fluid maintained at  $40 \text{ }^\circ\text{C}$ . Thermal conductivity,**

resistivity and convective heat transfer coefficient of the wire are 40 W/(m-deg), 50 micro-ohm-cm and 3500 W/(m<sup>2</sup>-deg) respectively.

**Solution:**

**Given: Length of wire = 3 m, Diameter of wire, d = 5 mm = 0.005 m**

**Current, I = 500 amp, Thermal conductivity, k = 40 W/ (m-deg),**

**Resistivity of wire, ρ = 50 micro-ohm-cm**

**Convective heat transfer coefficient, h = 3500 W/(m<sup>2</sup>-deg)**

**Temperature of fluid, T<sub>f</sub>=40°C,**

**To determine: i) Temperature at surface of wire, T<sub>2</sub>**

$$T_2 = T_f + \frac{q_g}{2h} r$$

$$\text{Electric resistance of wire, } R_e = \frac{\rho L}{A} = \frac{50 \times 10^{-6} \times 300}{\frac{\pi}{4} \times (0.5)^2} = \mathbf{0.076 \Omega}$$

$$\text{Volume of wire, } V = \frac{\pi}{4} d^2 L = \frac{\pi}{4} \left( \frac{5}{1000} \right)^2 \times 3 = 5.9 \times 10^{-5} \text{ m}^3$$

Heat generated per unit volume,

$$q_g = \frac{I^2 R_e}{\text{volume of wire}} = \frac{500^2 \times \mathbf{0.076}}{5.9 \times 10^{-5}} = 3.22 \times 10^8 \text{ W/m}^3$$

$$\text{Radius of wire, } r = \frac{5/2}{1000} = 0.0025 \text{ m}$$

Therefore, wire surface temperature

$$T_2 = T_f + \frac{q_g}{2h} r = 40 + \frac{3.22 \times 10^8}{2 \times 3500} \times 0.0025 = 40 + 115.18 = \mathbf{155.18^\circ C}$$

**ii) Maximum Temperature of wire, T<sub>max</sub>**

Maximum temperature in the wire occurs at its geometric centre line, and can be computed from the relation,

$$T_{max} = T_f + \frac{q_g}{2h} r + \frac{q_g}{4k} r^2$$

As  $T_2 = T_f + \frac{q_g}{2h} r$ , the above equation may be written as

$$T_{max} = T_2 + \frac{q_g}{4k} r^2$$

$$= 155.18 + \frac{3.22 \times 10^8}{4 \times 40} \times (0.0025)^2 = 155.18 + 12.59 = \mathbf{167.77^\circ C}$$

**Ex 6.6**

**An copper wire of diameter 10 mm and having electrical resistance of 0.075 ohm/km is carrying a current of 1000 amperes. Thermal conductivity of copper is 400 W/m-K and convective heat transfer coefficient for heat**

transfer from the wire surface to the surroundings is 20 W/m<sup>2</sup>-K. If the surrounding are at a temperature of 30°C determine for 1km length of wire

- (i) Rate of heat generation per unit volume of the wire.
- (ii) Maximum Temperature and Surface Temperature of copper wire

**Solution**

**Given: Length of wire, L = 1 km= 1000 m, Diameter of wire, d = 10 mm = 0.01 m**

**Current, I = 1000 amp, Thermal conductivity, k = 400 W/ (m-K),**

**Electrical Resistance of wire, R<sub>e</sub> = 0.075 ohm/ km**

**Convective heat transfer coefficient, h = 20 W/(m<sup>2</sup>-K)**

**Temperature of fluid, T<sub>f</sub>=30°C = 30+273=303**

**To determine: i) Rate of heat generation per unit volume of wire, q<sub>g</sub>**

$$q_g = \frac{I^2 R_e}{\text{volume of wire}} = \frac{1000^2 \times 0.075}{\frac{\pi}{4} \times 0.01^2 \times 1000} = 9.5 \times 10^5 \text{ W/m}^3$$

**ii) Surface Temperature and Maximum Temperature of wire, T<sub>max</sub>**

$$\text{Surface Temperature, } T_2 = T_f + \frac{q_g r}{2h} = 303 + \frac{9.5 \times 10^5}{2 \times 20} \times \frac{0.01}{2} = 303 + 112.5 = 415.5 \text{ K}$$

$$T_{max} = T_f + \frac{q_g r}{2h} + \frac{q_g r^2}{4k}$$

As  $T_2 = T_f + \frac{q_g r}{2h}$ , the above equation may be written as

$$\begin{aligned} T_{max} &= T_2 + \frac{q_g r^2}{4k} \\ &= 415.5 + \frac{9.5 \times 10^5}{4 \times 400} \times (0.01/2)^2 = 415.5 + 0.0148 = 415.51 \text{ K} \end{aligned}$$

The small difference between surface and maximum temperature occurring at centre of wire is on account of high thermal conductivity of copper and small heat generation rate.

**Ex 6.7** The inner and outer surfaces of a hollow cylinder are maintained at 500 °C and 475 °C by a heat source which is generating heat at a rate of 7× 10<sup>6</sup>w/ m<sup>3</sup>. If inner and outer radii of the cylinder are 2 cm and 3.5 cm respectively and thermal conductivity of the cylinder material is 20 W/m-deg, determine temperature at mid radius of the cylinder.

**Solution**

**Given: Inner radius of cylinder, r<sub>i</sub> = 2 cm = 0.02 m,**

**Outer radius of cylinder, r<sub>o</sub> = 3.5 cm = 0.035 m**

**Mid radius of cylinder,  $r_m = 0.027$  m**

**Thermal conductivity,  $k = 20$  W/ (m-deg),**

**Temperature of inner surface,  $T_1 = 500^\circ\text{C}$**

**Temperature of outer surface,  $T_2 = 475^\circ\text{C}$**

**Heat eneration rate,  $q_g = 7 \times 10^6 \text{w/m}^3$**

**To determine: i) Temperatur at mid radius of cylinder**

For the specified boundary conditions, the temperature distribution is given by

$$T - T_1 = \frac{q_g}{2k} (r_1^2 - r_m^2) + \left[ (T_1 - T_2) - \frac{q_g}{4k} (r_2^2 - r_1^2) \right] \frac{\log_e(r_m/r_1)}{\log_e(r_1/r_2)}$$

Inserting the appropriate data,

$$\begin{aligned} T - 500 &= \frac{7 \times 10^6}{4 \times 20} (0.02^2 - 0.027^2) \\ &+ \left[ (500 - 475) - \frac{7 \times 10^6}{4 \times 20} (0.035^2 - 0.02^2) \right] \frac{\log_e(0.027/0.02)}{\log_e(0.02/0.035)} \\ &= -28.78 + (25 - 72.18) \times \frac{0.3}{(-0.56)} = -3.505 \end{aligned}$$

∴ Temperature at mid radius,  $T = 500 - 3.505 = 496.495^\circ\text{C}$